



# 5th EURASIA WASTE MANAGEMENT SYMPOSIUM

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## Evaluation of Phosphogypsum as a Secondary Resource: Effect of Commercial Acid Treatment on Purification Efficiency

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### Abstract

Phosphoric acid is mainly produced via wet process method, based on the dissolution of phosphate ore in sulphuric acid. Phosphogypsum (PG) is a by-product of wet process, being generated 5 tons per 1 ton phosphoric acid. PG has an estimated 200-280 Mton of generation rate annually, only 15% being recycled and the rest 85% amount of untreated PG piles occupy large amounts of landfills. These PG piles attract attention in terms of environmental concerns, promoting searching of new alternative recycling processes. Valorization of PG as construction material offers a promising solution since it allows continuous consumption of PG stacks. Studies searching for a sustainable recycling of PG are generally conducted in cement industry. However, containing of a considerable amount of  $SO_4$  groups makes PG unsuitable for re-use in cement industry, since excess  $SO_4$  groups further react with  $C_3A$  (tricalcium aluminate phase) during hydration of cement. This study focuses on the determination of optimum washing parameters of PG in terms of  $SO_4$  removal. Washing experiments were conducted with  $H_2SO_4$  pre-treatment, then water. It was concluded that  $SO_4$  removal from PG can be effectively carried out with  $H_2SO_4$  treatment, making PG a suitable material for use in cement industry.

**Keywords:** Phosphogypsum, Re-use, Sustainability, Purification

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### 1. INTRODUCTION

Phosphoric acid is the main raw material in commercial phosphate-based fertilizer production. More than 90% of phosphoric acid is produced via wet process. Wet process phosphoric acid production can be explained as the dissolution of phosphate ore in sulphuric acid, generating 5 tons of phosphogypsum (PG) per 1 ton of phosphoric acid. Although wet process phosphoric acid is economically feasible, its main disadvantage is the generation of huge amounts of PG. Obtained PG is generally stored as stockpiles without any further treatment, occupying large amounts of landfills exposed to the environment, thus PG stockpiles are gaining attention in terms of environmental concern [1,2]. Recycling of PG is mostly conducted as construction material such as roadbed material, set retarder for cement, plaster board manufacturing etc [3]. However only 15% of PG is being recycled, rest 85% is stored without any further treatment due to its heterogenous structure. PG can basically be defined as  $(CaSO_4 \cdot 2H_2O)$  similar the gypsum but depending on the origin of the phosphate ore utilized in phosphoric acid manufacturing process PG can also contain some impurities such as heavy metals, rare earth elements, fluorides, sulphates and trace elements [4,5]. Containing of considerable amount of  $SO_4$

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groups makes PG unsuitable for re-use in cement industry, since excess  $SO_4$  groups further react with  $C_3A$  (tricalcium aluminate phase) during hydration of cement. In this study, PG samples were pre-treated with  $H_2SO_4$ , followed by washing with water. After filtration, cake samples were characterized with ICP-OES. According to results it is concluded that  $SO_4$  removal from PG can be effectively carried out with  $H_2SO_4$  treatment, making PG a suitable material for use in cement industry.

## 2. EXPERIMENTAL

PG sample was provided by a local fertilizer manufacturer. Sulfuric acid solution was prepared via a ready-to-use kit (Merck Titrisol 109981 Sulfuric acid). Ultrapure water (UPW) was prepared in Merck Millipore Direct-Q 8 UV Remote Water Purification System.  $SO_4$  content of samples were measured with Agilent 5110 ICP-OES.

0.5 M sulfuric acid solution was prepared with Merck Titrisol ready to use kit. Prior to washing procedure, PG samples were pre-treated with 0.5 M  $H_2SO_4$  solution in 1:10 and 1:20 solid:liquid ratios. After addition, experiment sets were stirred, sample taken and filtered. Acid treated PG was further washed with UPW in 1:10 and 1:20 solid:liquid ratios in both 500 and 1500 rpm mixing rates.

## 3. RESULTS & DISCUSSION

Untreated solid PG sample contains 15.4 wt %  $SO_4$ . According to results of dilute conditions (1:20 of solid:liquid ratio) and rapid stirring rate (1500 rpm) experiments, remaining  $SO_4$  in PG sample is measured as 0.8 wt %. Maximum  $SO_4$  removal from solid PG sample is calculated as 94.7%

## 4. CONCLUSIONS

In this study, PG sample is pre-treated with 0.5 M  $H_2SO_4$  and then washed with water in order to observe the effect of commercial acid treatment on  $SO_4$  removal efficiency. After acid treatment and washing, samples are filtered and  $SO_4$  amounts in washed PG cakes were measured with ICP-OES. According to results, dilute conditions and increased stirring rate increases  $SO_4$  removal efficiency.

## ACKNOWLEDGMENT

This study is financially supported by The Scientific and Technological Research Council of Turkey (TÜBİTAK, Project No: 118C085) and conducted between the co-operation of Ankara University and Toros AGRİ R&D Center within the scope of TÜBİTAK 2244 Industrial PhD Fellowship Program.

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## BIOGRAPHY



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